

CYCLE EFFICIENCY AND HEAT RATE OF THERMAL POWER PLANT

Prof. N R Sheth¹, Prof. Dhaval P Patel², Brijesh Patel³

¹ *Mechanical Engineering Department, Government Engineering College, Valsad, Email id*

² *Mechanical Engineering Department, Gandhinagar Institute of Technology, dhaval.patel@git.org.in*

³ *P G Student, Mechanical Engineering Department, Government Engineering College, Valsad, Email*

Abstract— The first law analysis of the coal fired thermal power station namely Gandhinagar Thermal Power Station (GTPS). In research paper, a detailed energy study is shown for 210MW, of coal fired thermal power plant at Gandhinagar Thermal Power Station (GTPS) to evaluate the plant and subsystem [feed water heaters (high pressure and low pressure)], etc. efficiencies. Cycle efficiency and heat rate are calculated using thermodynamic relation after estimating the various heat losses in the boilers, turbine and generator. Researcher gives suggestion for reduced heat losses in different components of power plant by applying Transport Membrane Condenser (TMC) in between boiler and condenser. Using TMC system which gives collect energy of flue gases and heated water directly bled in boiler which increase boiler efficiency.

Keywords- Power generating plant, boiler, steam turbine, first law analysis, Transport Membrane Condenser.

I. INTRODUCTION

In a coal based power plant coal is transported from coal mines to the power plant by railway in wagons or in a merry-go-round system. Coal is unloaded from the wagons to a moving underground conveyor belt. This coal from the mines is of no uniform size. So it is taken to the Crusher house and crushed to a size of 20mm. From the crusher house the coal is either stored in dead storage (generally 40 days coal supply) which serves as coal supply in case of coal supply bottle neck or to the live storage (8hours coal supply) in the raw coal bunker in the boiler house. Raw coal from the raw coal bunker is supplied to the Coal Mills by a Raw Coal Feeder. The Coal Mills or pulverizer pulverizes the coal to 200 mesh size. The powdered coal from the coal mills is carried to the boiler in coal pipes by high pressure hot air. The pulverized coal air mixture is burnt in the boiler in the combustion zone [10].

Generally in modern boilers tangential firing system is used i.e. the coal nozzles/guns form tangent to a circle. The temperature in fire wall is of the order of 1300deg.C. The boiler is a water tube boiler hanging from the top. Water is converted to steam in the boiler and steam is separated from water in the boiler Drum. The saturated steam from the boiler drum is taken to the Low Temperature Super heater, Platen Super heater and Final Super heater respectively for super heating. The super-heated steam from the final super heater is taken to the High Pressure Steam Turbine (HPT). In the HPT the steam pressure is utilized to rotate the turbine and the resultant is rotational energy. From the HPT the out coming steam is taken to the Reheater in the boiler to increase its temperature as the steam becomes wet at the HPT outlet. After reheating this steam is taken to the Intermediate Pressure Turbine (IPT) and then to the Low Pressure Turbine (LPT). The outlet of the LPT is sent to the condenser for condensing back to water by a cooling water system. This condensed water is collected in the hot well and is again sent to the boiler in a closed cycle. The rotational energy imparted to the turbine by high pressure steam is converted to electrical energy in generator [10].

Generator efficiency is taken as 98% so, the overall efficiency [3]

$$\eta_{\text{overall}} = (\text{boiler efficiency} * \text{turbine efficiency} * \text{generator efficiency})$$

$$\eta_{\text{overall}} = (0.8511 * 0.435 * 0.98)$$

$$\eta_{\text{overall}} = 36.28\%$$

Due to the turbine efficiency and boiler efficiency, we get overall efficiency is 36.28% i.e. is very low. The efficiency of the turbine is determined estimating the net heat input to turbine and electrical power plant from the generator in terms of heat values. Thus turbine efficiency obtained is 44.11%. The above results are shown in the table shown below:

Table 1 Result Summary: Cycle Efficiency

| CYCLE | EFFICIENCY (%) |
|--------------------------|----------------|
| CARNOTEFFICIENCY | 54.95 |
| THERMAL EFFICIENCY | 33.60 |
| OVERALL CYCLE EFFICIENCY | 36.28 |

Table 2 Result Summary: Components

| COMPONENT | EFFICIENCY (%) |
|--------------|----------------|
| BOILER | 85.11 |
| TURBINE | 44.11 |
| GENERATOR | 98 |
| OVERALLCYCLE | 36.28 |

III. HEAT RATE

TURBINE HEAT RATE[9][10]

Table 3 Turbine Steam-Water Data

| Sr. No. | Tag No. | Description | Value | Unit |
|---------|---------|-----------------------------------|-------|--------------------|
| 1.1 | FMST | Main steam flow turbine | 692 | T/hr |
| 1.2 | MWG | Megawatt Generated | 206 | MW |
| 1.3 | PMST | Main Steam Pr. At turbine inlet | 132.2 | Kg/cm ² |
| 1.4 | TMST | Main Steam Temp. At turbine inlet | 528 | °C |
| 1.5 | PFW | Feed water Pr. At Eco. Inlet | 154 | kg/cm ² |
| 1.6 | TFW | Feed water Pr. At Eco. Inlet | 238.5 | °C |
| 1.7 | PHRH | HRH Pr. | 33.7 | Kg/cm ² |
| 1.8 | THRH | HRH Temp. | 360 | °C |
| 1.9 | PCRH | CRH Pr. | 37.07 | |
| 1.10 | TCRH | CRH Temp. | 360 | °C |
| 1.11 | FRHS | Re heater Spray flow(L+R) | 8 | T/hr |
| 1.12 | FFW | Feed flow at Eco. Inlet | 625 | T/hr |
| 1.13 | PEH6 | Extraction Pr. Q THPH6 inlet | 37.07 | Kg/cm ² |
| 1.14 | TEH6 | Extraction Temp. Q THPH6 inlet | 360 | °C |
| 1.15 | TDH6 | Drain Temp. at HPH6 | 206.5 | °C |
| 1.16 | TFWHO6 | Feed water Temp. at HPH6 outlet | 239.2 | °C |
| 1.17 | TFWHI6 | Feed water Temp. at HPH6 inlet | 196.2 | °C |
| 1.18 | PBFD | BFP HDR Pr. | 171 | Kg/cm ² |

Note:-The pressure unit in Instrument is in Kg while in Steam table it is in bar. Hence conversion factor is $1 \text{ Kafka/cm}^2 = 0.98 \text{ bar}$ similarly in steam table enthalpy unit is KJ/Kg while we need enthalpy unit in Kcal/Kg. hence conversion factor is $\text{KJ} = 1/4.86 \text{ Kcal}$

Table 4 Turbine: Enthaply from Steam table

| Sr. No. | Tag No. | Description | Equation | Result (kcal/kg) |
|---------|---------|--------------------|---------------------|------------------|
| 2.1 | HMST | ENTH MSTOTURB | F(PMST, TMST)#ST | 816.85 |
| 2.2 | HFW | ENTH FWTOECONINLET | F(PFW, TFW)#ST | 246.13 |
| 2.3 | HHRH | ENTH HRHSTM | F(PHRH, THRH) #ST | 840.70 |
| 2.4 | HCRH | ENTH CRHSTM | F(PCRH, TCRH) #ST | 752.36 |
| 2.5 | HEH6 | ENTH EXTSTMTTOHPH6 | F(PEH6, TEH6) #ST | 752.36 |
| 2.6 | HDH6 | ENTH HPH6DRN | F(PEH6, TDH6) #ST | 210.63 |
| 2.7 | HFWHO6 | ENTH FWHPH6OUT | F(PBFD, TFWHO6) #ST | 247.12 |
| 2.8 | HFWHI6 | ENTH FWHPH6IN | F(TPBD, TFWHI6) #ST | 199.52 |

CALCULATION OF HEAT RATE[3][4]

FEH6 = Flow of Extraction steam to HPH6

$$FEH6 = FFW * (HFWHO6 - HFWHI6) / (HEH6 - HDH6)$$

$$= \frac{\text{Feed flow to eco. inlet} * (\text{Enthalpy of FW of HPH6 outlet} - \text{Enthalpy of FW of HPH6 inlet})}{(\text{Enthalpy of Extraction Steam of HPH6} - \text{Enthalpy of Drain water of HPH6})}$$

$$= \frac{625 * (247.12 - 199.52)}{(752.36 - 210.63)}$$

$$= \frac{625 * 47.6}{541.73}$$

FEH6 = 54.91 T/hr

FHRH = HRH Flow

$$= FHRH = FMS - FEH6 + FRHS$$

$$= (\text{Total Main Steam flow} - \text{flow of extract .steam to HPH6}) + (\text{Total reheater spray flow})$$

$$= (692 - 54.91) + 8$$

FHRH = 645.09 T/hr

QT = Heat input to Turbine Cycle

$$= FMST (HMST - HFW) * 1000 + FHRH (HHRH - HCRH) * 1000$$

$$= \text{Hot Reheat flow} * (\text{Enthalpy of HRH steam} - \text{Enthalpy of HCRH Steam}) * 1000$$

$$= 692 * (816.85 - 246.13) * 1000 + 645.09 * (840.70 - 752.36) * 1000$$

$$= 692 * 570.72 * 1000 + 645.09 * 88.34 * 1000$$

$$= 451925490 \text{ Kcal/ hr}$$

QT = 451925.49 * 1000 Kcal/ hr

Turbine Heat Rate = QT/1000 * MWG

Where, MWG = MW generated = 206 MW

$$= 451925.49 * 1000 / 206 * 1000$$

$$= 2193.81 \text{ Kcal/KWh}$$

Hence, Turbine Heat Rate = 2193.81 Kcal/KWh

STATION HEAT RATE

Station heat rate is to be calculated by following formula,

$$\text{Station heat rate} = \frac{\text{Turbine cycle heat rate}}{\text{Boiler efficiency}\%} * 100$$

$$= \frac{2193.81 \text{ Kcal/KWh}}{0.8511}$$

Station heat rate = 2577.6172 Kcal/KWh

NET-HEAT RATE

Net-Heat rate i.e. plant heat rate can be calculated as follows,

$$\text{Net heat rate} = \frac{\text{Fuel flow (kg/hr)} * \text{Fuel heating value (Kcal/Kg)}}{\text{Net Power Output (KW)}}$$

$$= \frac{125000 * 4097}{210000}$$

Net heat rate=2438.6904 Kcal/KWh

IV. RESULTS

| Heat rate | Result (Kcal/KWh) |
|-------------------|-------------------|
| Turbine Heat rate | 2193.81 |
| Station Heat rate | 2577.61 |
| Net Heat rate | 2438.69 |

V. TWO-STAGE TMC INTEGRATION WITH A POWER PLANT

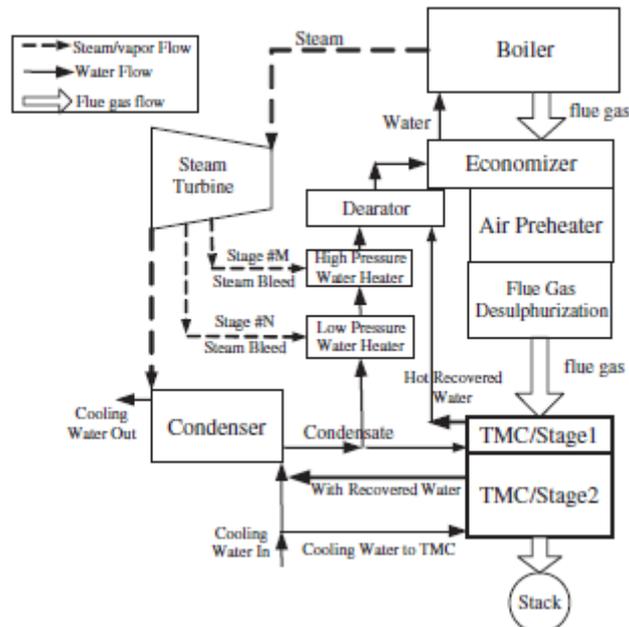


Figure 2 Two-stage TMC integration with a power plant

Fig. 2 shows a schematic for integrating the TMC water recovery unit in a typical power generation boiler and steam turbine loop. For the two-stage TMC unit to maximize its function for recovering both water and heat, two separate cooling water streams are used. On the water side, the first-stage TMC inlet water will be obtained from steam condensate from the condenser, and its outlet water with recovered water vapor and associated latent heat from flue gas will go to the deaerator for boiler water makeup. The second stage TMC inlet water will be part of the condenser cooling water stream. The outlet water from this TMC stage will

then be routed to go back to the cooling water stream with extra recovered water from the flue gas. On the flue gas side, the TMC is situated between the FGD unit and the stack. [15]

VI. CONCLUSION

From the energy analysis made for the unit-4,210MW of the GTPS – the following conclusion are drawn:

- From the thermodynamic analysis using first law of thermo dynamics, we can conclude that, energy analysis evaluates the plant quantitatively. The power plant overall efficiency is 36.28%.
- Lower the heat rate, higher the cycle efficiency. Here, net heat rate at full load is to be 2438.69 Kcal/KWh.
- If TMC system implement in thermal power plant it will increase boiler efficiency then effect of TMC reduced heat losses in plant so overall thermal efficiency plant will increase.

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